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1 **Atomisation gas type, device configuration and storage conditions strongly**  
2 **influence survival of *Lactobacillus casei* after spray drying**

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## Abstract

Many pathologies are characterised by an imbalance between the beneficial bacteria and potentially pathogenic microbes, i.e. dysregulated host/microbial interactions. Probiotic bacteria are increasingly explored for regulation of immune responses and restoring this imbalance. The application of probiotics most commonly involves drying in formulation development, that can potentially reduce their viability and functionality, hence different protective strategies are needed. Here, spray drying was used for probiotic preservation and effects of device configuration, oxygen injury and encapsulation with increasing skim milk concentrations, were studied on the survival of *L. casei* AMBR2. Quantitative analysis showed no significant differences on bacterial viability for spray drying in an open versus closed system whilst spray drying in a co-current gas flow. Addition of the anti-oxidant, ascorbic acid, to the drying medium adversely impacted viability. Also, no benefits of nitrogen spray drying were observed, implying that oxygen-induced damage is not significant in this setup, at least for the specific tested strain. Additionally, this work shows how storage conditions and total feed solid content significantly alter spray drying viability outcomes. Spray drying was able to retain the high viability of cells of  $10^9$  CFU/g and higher after 52 weeks at refrigerated storage, whereas  $10^6$  CFU/g were maintained at room temperature. This study favours air over nitrogen-based spray drying and confirms the method suitability for high viability retention over a year of shelf-life.

**Key words:** spray drying, nitrogen, processing, stability, inert loop, skim milk, ascorbic acid

## 45 **1. Introduction**

46 Lactic acid bacteria (LAB) are a group of widely studied beneficial microorganisms,  
47 extensively used in food industry, pharmaceuticals, for agricultural purposes. Among the LAB,  
48 members of the *Lactobacillus casei* group, recently revised as the *Lacticaseibacillus* genus,  
49 are perhaps most commonly applied with significant commercial value [1, 2]. The focus on the  
50 group's members and their significance is particularly in context of functional foods and  
51 pharmabiotics [2]. Recently, a novel human derived strain, *L. casei* AMBR2, was isolated and  
52 characterised for its potential application in various spheres as a probiotic [3, 4]. Probiotics are  
53 “live microorganisms that, when administered in adequate amounts confer a health benefit on  
54 the host” [5]. To exert a health benefit on the host, probiotics typically need to be applied in  
55 the amount of  $10^7$ - $10^8$  CFU/mL, although the required dose can be strain, formulation and  
56 application dependent, with applications outside the gut generally requiring lower doses [6]. In  
57 order to meet these standards, an economically feasible production tailored to the specific strain  
58 and targeted application is needed. Therefore, spray drying is an attractive low-cost, flexible  
59 alternative to conventional freeze-drying for the probiotic product manufacturing at many  
60 different scales. It is being increasingly explored for the formulation of probiotics and other  
61 bioactives for multiple applications, also outside the gastro-intestinal tract where spray-dried  
62 powder can have superior characteristics compared to freeze-dried powder [7–11].

63 Loss of bacterial viability after spray drying has been many times documented [12–16].  
64 Cell injury is attributed primarily to inlet and outlet heat, feed moisture content, dehydration  
65 and osmotic stress, but also atomisation and oxidative damage [17, 18]. Additionally, various  
66 strategies such as adjustment of cell number inputs, bacterial growth phase in the moment of  
67 processing, modelling approach, studying drying kinetics and kinetics of cell death etc. have  
68 been proposed for the optimisation of process parameters towards the retention of probiotic  
69 properties and better probiotic survival [17–22]. The impact of atomisation gas type and loop

70 configuration influence upon bacterial viability, powder characteristics, and process scalability  
71 for an industrial application are usually overlooked. Laboratory scale spray dryers are  
72 commonly used in an open loop system, meaning that additional optimisation for the industry  
73 size production is needed in terms of cost, efficiency and environmental issues [23]. Moreover,  
74 atomisation gas type may influence partitioning of sample feed (feed to be dried) into droplets,  
75 regarding droplet size, droplet velocity and consequently affect the properties of the end  
76 product - powder [23, 24]. Typically, for aqueous feed suspensions, air is used, but for non-  
77 aqueous feed, inert gases such as nitrogen and helium, are employed. Depending on the feed  
78 solution/suspension composition, the aimed level of crystallinity of the final powder, switching  
79 drying gas from air to nitrogen or other gases could provide a significant improvement [24].  
80 Moreover, depletion of oxygen from spray drying process could limit probiotic cell damage  
81 originating from reactive oxygen species (ROS) [25]. This is potentially dependent on the  
82 inherent oxidative stress resistance capacities of the probiotic strains used, because some strains  
83 express catalase or super oxide dismutase enzymes that can mitigate ROS [3], especially  
84 considering that viability and activity after spray drying are vastly strain-specific [7].

85 Various studies on probiotic preservation by air spray drying for food and  
86 pharmaceutical application are available, however a little is known about the use of the inert  
87 loop spray drying system and inert gases as carriers [26–29]. Therefore, this study aimed to  
88 compare the impact of inert loop spray drying and inert gases as carriers on the bacterial  
89 viability and powder properties of the model respiratory tract probiotic *Lactocaseibacillus casei*  
90 AMBR2 [7]. Next, the influence of the system configuration as well as the addition of  
91 antioxidants were tested on bacterial viability. Additionally, enhancing the viability of the  
92 chosen bacterial strain for more than a year using skim milk (SM) as a model excipient was  
93 investigated. Although milk by-products are widely used as good protective agents for spray  
94 drying of probiotics [30, 31], there is currently a lack of data on long-term stability of spray-

95 dried probiotic powders. Lastly, variation in storage viability in relation to the solid content -  
96 excipient amount, and storage conditions was evaluated via four different formulations.

## 97 **2. Materials and methods**

### 98 **2.1 Cultivation conditions and media composition**

99 *L. casei* AMBR2 LMG P-30039 was used in this study [4]. The strain was isolated from  
100 the upper respiratory tract (URT) of a healthy individual and has demonstrated properties of a  
101 potential (URT) probiotic. The documented presence of effector molecules, such as fimbriae,  
102 and its good adhesive properties to respiratory and gastro-intestinal epithelial cells could  
103 qualify it for applications besides URT. Stock cultures of AMBR2 were locally maintained in  
104 25% (v/v) aqueous glycerol at -80 °C. Cultivation was performed in the de Man, Rogosa and  
105 Sharpe (MRS) broth (Carl Roth, Mühlburg, Germany) till stationary phase of growth was  
106 reached when cells were harvested by centrifugation for 12 minutes at 3983 x g at 20 °C (Sigma  
107 3-16PK, Sigma Zentrifugen, Germany). To test the direct effects of device configuration  
108 demineralised water with or without addition of 0.05% (w/V) ascorbic acid (Fagron, Belgium  
109 NV.) was used. Next, water-based feed media such as 1%, 10% and 20% (w/V) SM (Oxoid,  
110 Thermo Fischer Scientific, Massachusetts, USA) including unprotected bacterial suspension  
111 (0%), as a control, were employed in shelf-life and method comparison tests. Briefly, SM was  
112 dispersed in demineralised water under magnetic stirring, until complete dissolution, under  
113 aseptic conditions. The centrifuged bacterial cells were re-suspended in prepared SM solutions.

### 114 **2.2 Spray drying**

115 Spray drying procedure was based on our previous findings [7, 20]. Laboratory-scale  
116 spray driers, B-290 and B-295 advanced inert loop containing oxygen sensor to detect oxygen  
117 levels in the system and dehumidifier (Büchi, Flawil, Switzerland) were used to process  
118 samples at constant processing parameters (135 °C inlet temperature, ~55 °C outlet

119 temperature, 7.5 mL/min flow and 32.5 m<sup>3</sup>/h gas flow rate). Two different gas carriers were  
120 evaluated, atmospheric air in both, open system and closed system, and nitrogen in the inert  
121 loop – also closed system. When air was used in a closed system, oxygen sensor within the  
122 inert loop was turned off to allow performance. Spray dryers had a co-current configuration  
123 and the same two-fluid nozzle was used (orifice diameter of 1.4 mm). After 15 minutes of spray  
124 drying the powder samples were collected directly from single cyclone separators.

### 125 **2.3 Long-term storage stability**

126 Dried powders of each formulation were stored in Eppendorf tubes (VWR International  
127 Europe, Leuven, Belgium), sealed with Parafilm® and kept at room temperature with and  
128 without light exposure and refrigerated conditions (4-8 °C) at an ambient relative humidity  
129 (RH). The cells' stability was evaluated after predefined intervals of 1, 4, 28 and 52 weeks.

### 130 **2.4 Enumeration of viable cells**

131 Viability before spray drying, taken as the initial count, and after spray drying and  
132 storage were estimated via serial dilutions plated out onto MRS agar (Carl Roth, Mühlburg,  
133 Germany) plates in triplicate. Spray-dried powders of each batch prior serial diluting were re-  
134 suspended in adequate amounts of demineralised water, to the initial concentration before  
135 drying, at room temperature. Incubation of inoculated plates was done at 37 °C for 48h and  
136 plates containing 30 – 300 colonies were chosen for counting the viable cells.

137 Viability rate after spray drying was determined as a comparison between colony  
138 forming unit (CFU) counts before spray drying and CFU counts in powders rehydrated to the  
139 same solid content / water ratio as before spray drying. The data was expressed in CFU/g as  
140 mean value ± standard deviation. The same methodology was applied during the determination  
141 of bacterial viability after long-term storage under different conditions.

142        **2.5 Powder morphology**

143            The morphology of *L. casei* AMBR2 probiotic powders was visualised by scanning  
144 electron microscopy using a Quanta FEG250 SEM system (Thermo Fisher, Asse, Belgium).  
145 The powders were mounted on SEM stubs using conductive carbon tapes. The stubs were  
146 sputter-coated with gold (10 nm) and imaged at a voltage of 5 kV.

147            Particle size was measured using the laser diffraction technique (Malvern 3000,  
148 Malvern Instruments Ltd., Malvern, UK) in dry conditions in a small sample device. The size  
149 was calculated in accordance with the Mie theory of light scattering and reported as a volume  
150 equivalent sphere diameter.

151        **2.6 Moisture content**

152            Karl-Fisher Titration (Karl-Fisher Titrino Plus, Metrohm Germany) was used to  
153 measure water content of spray-dried powders. Analyses were carried out in 100-200 mg of  
154 spray-dried powder at room temperature with Aqualine Composite 5 (Fisher Scientific, UK)  
155 with constant stirring.

156        **2.7 Differential scanning calorimetry**

157            The thermal properties of the spray-dried powder samples were determined using a  
158 Discovery DSC25 equipment from TA Instrument (New Castle, DE, USA). Powder samples  
159 (5–10 mg) were analysed in Tzero aluminum pans under 50 mL/min nitrogen gas purge in  
160 modulated temperature mode. The enthalpy and temperature was calibrated using an indium  
161 standard and the heat capacity was calibrated using a sapphire standard. All samples were  
162 heated from -40 to 270 °C at a 2 °C/min heating rate with a modulation of 1.6 °C/min.  
163 Determination of the melting peak and glass transition temperature was performed using the  
164 TA Instruments TRIOS software.

165        **2.8 Yield, bulk density and powder flowability**

166            Yield was defined as the ratio of the amount of the dried powder vs. amount of solids  
167 in the bacterial suspension subjected to spray drying.

168            Yield (%)= weight of spray-dried powder (g)/ weight of solids before drying x 100

169            Bulk density of spray-dried probiotic powders was determined using the method  
170 described by Arepally et al. [32]. The measurements were conducted in a 10 mL graduated  
171 cylinder using the tap density tester PT-TD200 (Pharmatest, Germany). The loose and tapped  
172 bulk density of spray-dried powder was calculated using the following formulas respectively:

- 173            • Loose bulk density (g/cm<sup>3</sup>) = weight of powder (g)/bulk powder volume (cm<sup>3</sup>)
- 174            • Tapped bulk density (g/cm<sup>3</sup>) = weight of powder (g)/tapped powder  
175            volume(cm<sup>3</sup>)

176            Hausner ratio (HR) was used to estimate the flowability of spray-dried probiotic  
177 powders. Table1 illustrates the guidelines for the HR that were used in the result evaluation.  
178 Hausner ratio was calculated as follows:

179            Hausner ratio = tapped bulk density (g/cm<sup>3</sup>)/loose bulk density (g/cm<sup>3</sup>)

180        **2.9 Statistical analysis**

181            Statistical significance of the differences between obtained powders was checked with  
182 SPSS 26 software (IBM statistics, New York, USA) using two-way or one-way ANOVA-test  
183 and Tukey's multiple comparisons test. Significance level of  $\alpha=0.05$  was applied. All  
184 experiments were performed at least three times. Data are expressed as means  $\pm$  standard  
185 deviation or as means.

### 186 3. Results

#### 187 3.1 *Impact of gas type, device configuration and antioxidant fortification*

188 The viability of *L. casei* AMBR2 was examined via the net effect of different device  
189 configurations, *i.e.* open and closed system, different gas carriers, with and without the  
190 presence of ascorbic acid (Figure 2). Interestingly, comparable viability (with 0.5 log reduction  
191 in viability) was obtained when cells were dried in an open and closed mode using atmospheric  
192 air as a carrier. Contrarily to what we expected, the addition of ascorbic acid (vitamin C) as an  
193 oxygen scavenger to reduce and prevent oxidative damage of cells, actually resulted in a  
194 significant decrease in CFU counts in both open and closed air-based systems (0.80 and 1 log  
195 reduction CFU, respectively). Furthermore, the oxygen depletion by using a 99.5% nitrogen as  
196 a gas carrier also resulted in a significantly lower CFU numbers in comparison to the air carrier  
197 systems. Vitamin C fortification of the suspensions dried in the nitrogen inert and closed system  
198 also did not result in an improved survival, yet in similar outcomes as without any additions,  
199 or a 0.85 log reduction.

#### 200 3.2 *Effect of excipient amount on viability and powder properties after air and nitrogen* 201 *spray drying*

202 Figure 3A shows that addition of increasing SM amounts to the feed suspension media  
203 led to an expected increase in bacterial survival in both air and nitrogen spray drying. This  
204 increase was statistically significant for all three SM concentrations when nitrogen spray drying  
205 was employed, whereas for air spray drying survival was improved significantly in 10% and  
206 20% SM formulations, but not in 1% formulation. Our aim was to compare the two methods  
207 and their outcomes not only via viability quantification but also via powder characteristics after  
208 drying. As seen in Figure 3B, both methods resulted in powders with comparable  
209 characteristics such as drying yield, water content, flow properties, and density, in contrast to

210 rather different viability outcomes (Figure 3A). Drying yields were over 50% in majority of  
211 formulations, which is in alignment with the production feasibility [33]. Noticeable is low bulk  
212 density in all formulations, although its increase was recorded along with the increase in SM  
213 concentrations and consequent increase in total solid content of feed suspensions. Of note is  
214 that all formulations independently of the gas carrier had poor or very poor flow properties  
215 reflected in high Hausner's ratios. Importantly, although a desirably low water content, around  
216 4% [15], can be observed, its further decrease was also noticed with higher solid contents.  
217 Importantly, glass transition temperatures (T<sub>g</sub>s) were observed in thermograms of all samples  
218 except those dried without SM addition, where thermal degradation was visible, and  
219 corresponded to the literature values. However, these phase transitions events were only minor,  
220 and thus all formulations only partially amorphous, considering the presence of very sharp  
221 endothermic peaks at approx. 180 °C. These peaks correspond to the melting peak of lactose,  
222 the dominant component of SM [34] . Interestingly, a depression of T<sub>g</sub>s, i.e. slightly lower T<sub>g</sub>s  
223 than previously documented were observed in samples dried in the nitrogen system. Figure 3C  
224 shows particle size distributions of all tested formulations dried in both air and nitrogen  
225 indicating the increase in median particle size values ( $\sim D_x(50)$ ) (3.2  $\mu\text{m}$ , 3.5  $\mu\text{m}$ , 8  $\mu\text{m}$  and 10  
226  $\mu\text{m}$ , for 0%, 1%, 10% and 20% SM respectively) with the increase in SM solid content.  
227 Viability results after spray drying in both systems have shown a moderate correlation with the  
228 particle size values of corresponding formulations (Pearson's coefficient  $r=-0.68$ ). Next, Figure  
229 3D visualises the particles of all formulations (0%, 1%, 10% and 20% SM) formed by spray  
230 drying in both air and nitrogen systems. Here, yet again no major differences between the two  
231 techniques were observed. The particle appearance in samples dried without SM reflected  
232 interlinked cell agglomerates of different sizes, whereas formulations with SM resulted in  
233 coating of cells, i.e. irregularly shaped partially collapsed particles. Additionally, the coating  
234 was not complete when 1% SM was used, and some free cells were still visible, but 10% and

235 20% SM resulted in a complete cell encapsulation. The increase in particle size with the  
236 increase of SM concentration was also recorded by SEM.

### 237 *3.3 Effect of storage conditions upon shelf-life viability*

238 The impact of different storage conditions on bacterial viability over time at ambient  
239 RH is depicted in Figure 4. Visibly higher initial cell counts per gram in 0% and 1% SM than  
240 in 10% and 20% SM formulations do not indicate better survival, but originate from a much  
241 bigger matrix (solid content) with homogeneously embedded cells in the later formulations. A  
242 gradient decrease in viability was observed for all samples kept at room temperature. This  
243 decrease was especially prominent in samples kept at room temperature with daylight exposure.  
244 However, countable viability was still present in those samples but with the highest SM content  
245 at 28-week point. Regarding the samples kept without light exposure, their viability was  
246 countable at 52-week stability point only in case of 20% SM dried in both air and nitrogen. As  
247 expected for unprotected cells, their number ceased independently of the storage conditions  
248 and drying method and was not countable anymore after 28 weeks. Although, initially resulting  
249 in high viability numbers, 1% SM formulations had a steep loss of viability over time in both,  
250 room storage conditions and at refrigerated storage, where in spite of the significant loss had  
251 approx.  $10^5 - 10^6$  CFU/g at the time of the last evaluation. In contrast samples containing 10  
252 and 20% SM dried in air and nitrogen maintained very high viability at refrigerated storage for  
253 52 weeks,  $>10^9$  CFU/g of powder.

## 254 **4. Discussion**

255 In this study, we aimed to determine the importance and size of the oxidative cell injury  
256 originating from the oxygen present in the drying medium and oxygen dissolved in the  
257 suspension to be dried [35]. Removing oxygen from the drying medium and the addition of an  
258 oxygen scavenger such as ascorbic acid has been many times debated, however, experimentally

259 documented only in a limited number of cases [25, 36–38]. In contrast to findings of these  
260 studies, our research has shown a contradictory effect of the vitamin C feed suspension  
261 fortification (Figure 2). A potential explanation of this phenomenon can be that dehydration  
262 process itself leads to an increase in oxidative state of cells and production of ROS [35, 39]  
263 rather than ROS being introduced via drying medium. This in turn would mean that water  
264 depletion from cells during drying besides impacting DNA, RNA and proteins as a  
265 consequence has ROS generation that contributes to the additional lipid peroxidation, protein  
266 denaturation, etc. as demonstrated in eukaryotic cells [39, 40]. Also, of note is the dual nature  
267 of the ascorbic acid, on one side radical scavenger and on the other pro-oxidant that generates  
268 hydroxyl radicals that could oxidise biological molecules. Namely, its counter effect during  
269 storage stability of *Lactobacillus delbrueckii* ssp. *bulgaricus* was reported by Teixeira et al.  
270 [41] and on *Bifidobacterium longum* by Champagne et al. [42]. We extended this study and  
271 tested air spray drying in a closed system as well as nitrogen spray drying with the addition of  
272 ascorbic acid (Figure 2). Importantly, our results suggest that viability after spray drying in a  
273 closed system is equally good as in an open system, in spite of the anticipation of a slightly  
274 higher heat accumulation and different back pressures. The aspect of the device configuration  
275 is often neglected by authors or not clearly defined, although the configuration and glassware  
276 assembly type could potentially play an important role in this context as they play in  
277 mechanical forces generation and process optimisation. However, the extent of bacterial death  
278 increased when nitrogen was used as a drying gas contrasting findings of Ghandi et al. for  
279 *Lactococcus lactis* [25] and Wang et al. for *Bordetella pertussis* [43]. Underlying reasons for  
280 these outcomes are rather unclear, but could be attributed to the strain specific behaviour  
281 towards different stresses and different processing techniques. Our strain of choice should be  
282 indeed more oxidative stress resistant, but current results do not provide sufficient data on why  
283 a higher damage occurs when oxygen is diminished. Moreover, the strain's facultative

284 anaerobic nature would imply tolerance of both presence and absence of oxygen in any system.  
285 Combination of nitrogen and ascorbic acid has surprisingly led to a slight survival improvement  
286 in comparison to the nitrogen itself, but remained still significantly lower than survival in air-  
287 based systems (Figure 2).

288         Additionally, a long-term stability study with bacteria encapsulated with increasing SM  
289 solid content with varying storage conditions was conducted to further evaluate the differences  
290 between nitrogen and air spray drying (Figure 4). SM was chosen for the evaluation as milk  
291 proteins and their protective capacity in encapsulation of probiotic bacteria after spray drying  
292 and over time was documented by authors [30, 31, 44], and confirmed through our experiments.  
293 Also, the increase in SM concentrations, unlike when pure sugar protectants are used, has led  
294 to the proportional increase of particle size during encapsulation which could allow a proper  
295 evaluation of the significance of the solid content and particle size in shelf-life stability and  
296 spray drying (Figure 3C). SM beneficial effect raises from cell surface layer formation through  
297 hydrophobic reaction between cells and milk proteins resulting in a microcapsule formation  
298 [45]. Those microcapsules exhibit concavities (Figure 3D) because of processing at high  
299 temperatures that are believed to make particles stronger against fractures and solute diffusion  
300 [46] and have remained intact over time regardless of the storage condition (Supplement 1).  
301 Here, although viability results after spray drying were comparable among different SM  
302 concentrations (Figure 3A), over time the best viability was maintained with SM concentrations  
303 higher than 1%, probably due to more complete microcapsule formation as confirmed by SEM  
304 in Figure 3D. Correlation analysis has further shown a certain degree of dependency of the  
305 viability outcome and particle size, meaning that bigger particles usually led to better  
306 protection. According to Würth et al. [47] the size of SM microcapsules correlated negatively  
307 with the viability of *Lactobacillus paracasei* ssp. *paracasei* F19 due to longer retention times  
308 of bigger particles in the dryer. Yet, this was not confirmed in our study. Of note is that the

309 double increase in solid content from 10% to 20% SM overall neither led to a further viability  
310 improvement nor to a better shelf-life meaning that there are minimum needed and maximum  
311 necessary concentrations of the excipient (Figure 3A and Figure 4). When literature is browsed,  
312 much higher concentrations of SM and excipients in general may be seen (over 30% w/V),  
313 which is not cost-effective for an industrial scale production. On the other hand, considering  
314 very good protective power of SM, differences between air and nitrogen spray drying were not  
315 distinguishable as when no excipients were added. Important is to mention that powders  
316 obtained by both methods had overall similar characteristics in terms of yield, flowability, low  
317 bulk density, that increased with the increase in solid matter, and water content (Figure 3B).  
318 As reviewed by many authors [19, 48–50] main aspects important to consider for storage  
319 stability are temperature, oxygen content in packaging and moisture level of the product. Our  
320 findings confirm the importance of the storage temperature in preserving high bacterial  
321 viability over time where, as expected, refrigerated storage conditions resulted in the highest  
322 viability over time (~1 log reduction for all formulations of 10 and 20% SM after 52 weeks)  
323 (Figure 4). Similar was shown by Wanticha Lapsiri, Bhesh Bhandari and Penkhae  
324 Wanchaitanawong [51] with spray-dried *L. plantarum* TISTR 2075 whose survival during  
325 shelf-life was predominantly dependent on the storage temperature and RH, as well as by Reyes  
326 et al. [52] and 60 day-storage stability of *L. plantarum* NRRL B-4496. It is well-known that  
327 storage temperature should always be below the T<sub>g</sub> of the product to increase its stability and  
328 that moisture content plays a role in relation to it [48, 51]. However, although all of our  
329 powders were kept at temperatures below their T<sub>g</sub> the improvement was only significant at 4-  
330 8 °C, whereas we do observe better viability outcomes over shelf-life in samples with lower  
331 initial water content related to the increase in solid content of spray-dried suspensions. Hence,  
332 T<sub>g</sub> cannot be considered as a main inactivation point, since multiple causes underlie the storage  
333 death rate and progress [31]. Next, amorphous systems are in most of the times favourable over

334 crystalline or partly crystalline when it comes to the viability protection of bacteria over time,  
335 because glassy matrix, such as formed with sugars like lactose or trehalose, is believed to  
336 restrict molecular movements and slow down detrimental processes [28, 53]. Contrarily, our  
337 current and unpublished results do not stress the importance of material state, but rather  
338 formulation specific reactions between excipients and bacteria. Besides, Önnby et al. [54]  
339 reported the example of freeze dried *Sphingobium* sp. where complete loss of viability  
340 happened after 4 weeks in both amorphous and crystalline sugar matrices. When it comes to  
341 storage stability, it is plausible that light exposure could have a negative effect, due to UV rays  
342 causing DNA damages [55], which is quite visible in our results (Figure 4A). Moreover, the  
343 detrimental effect of the daylight was seen already after a couple of days and resulted in a very  
344 fast and steep decrease in viability during storage. This requires careful manipulation in  
345 downstream processing as well as special packaging requirements. As concluded by Tripathi  
346 et al. [55] next to light permeability of the packaging material, other aspects such as packaging  
347 technique, type of its material, i.e. glass or different types of plastic, could result in different  
348 shelf-lives especially because of different oxygen permeability. Thus, as suggested by the same  
349 author, glass packages with a hermetic closure should lead to more stable products which could  
350 be a potential solution for our formulations kept at room temperature in dark.

## 351 **5. Conclusions**

352 In conclusion, we found that addition of ascorbic acid in the feed suspension medium  
353 did not improve cell survival after spray drying as well as that drying in closed systems with  
354 recirculating gas results in comparable viability results as the open-system spray drying.  
355 Nitrogen gas carrier also did not result in an improved spray drying outcomes, although resulted  
356 in powders of similar characteristics as when atmospheric air was the carrier. Therefore, at least  
357 for *L. casei* AMBR2 oxidative damage during spray drying is not the main cause of the viability  
358 loss. SM provided high long-term viability protection at refrigerated storage while it's

359 concentration evaluation revealed no need for very high solid amounts to protect bacteria  
360 effectively. Our research has once again highlighted the influence of storage conditions upon  
361 shelf-life probiotic viability. Although our results favour air spray drying, nitrogen can find its  
362 application for more oxygen sensitive microorganisms and their preservation.

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## 371 **7. Conflict of interest**

372 None.

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581 **Figure 1** Device configuration, open system (A), closed system (B)

582 **Table 1** The Hausner ratio as a scale of flowability; European Pharmacopoeia 9.8, 2.9.36  
583 Powder Flow, 01/2010

584 **Figure 2** Log reduction after spray drying of unprotected *L. casei* AMBR2 cells using air as a  
585 carrier: in an open system (AO), in a closed system (AC), in an open system with presence of  
586 vitamin C in feed suspension medium (AOC), in a closed system with presence of vitamin C  
587 in feed suspension medium (ACC); log reduction in viability after spray drying of unprotected  
588 cells using nitrogen as a gas carrier (N), and with vitamin C addition to feed suspension medium  
589 (NC). Stars (\*) indicate the level of statistical significance (one-way ANOVA-test and Tukey's  
590 multiple comparisons test,  $p < 0.05$ ).

591 **Figure 3** Comparison of log reduction of *L. casei* AMBR2 when dried in absence of protectants  
592 (0%), 1%, 10% and 20% (w/V) SM in both air and nitrogen (A) where stars indicate the level  
593 of statistical difference significance (two-way ANOVA-test and Tukey's multiple comparisons  
594 test,  $p < 0.05$ ). Powder characteristics of AMBR2 spray-dried formulations of unprotected cells  
595 (0%) and 1%, 10% and 20% SM dried in both, air and nitrogen gas stream (B), particle size  
596 distribution of all formulations (C), scanning electron micrographs of AMBR2 formulations  
597 (D) in absence of protectants dried in air (a) and in nitrogen (e), in 1% SM dried in air (b) and  
598 in nitrogen (f), in 10% SM dried in air (c) and in nitrogen (g), in 20% SM dried in air (d) and  
599 in nitrogen (h).

600 **Figure 4** Shelf-life viability up to 52 weeks at room temperature with daylight exposure (A),  
601 at room temperature without daylight exposure (B) and at refrigerated conditions (C) of *L. casei*  
602 AMBR2 unprotected cells (0%) and protected with 1%, 10% and 20% (w/V) SM dried in air  
603 open system (air) and nitrogen system (nitrogen).

604 **Supplement 1** Scanning electron micrographs of *L. casei* AMBR2 spray-dried powders after  
605 28 weeks of shelf-life dried in air: unprotected cells kept at room temperature with daylight  
606 exposure (a1), at room temperature without daylight exposure (a2), at refrigerated conditions  
607 (a3), 1% SM formulation cells kept at room temperature with daylight exposure (b1), at room  
608 temperature without daylight exposure (b2), at refrigerated conditions (b3), 10% SM  
609 formulation cells kept at room temperature with daylight exposure (c1), at room temperature  
610 without daylight exposure (c2), at refrigerated conditions (c3), 20% SM formulation cells kept  
611 at room temperature with daylight exposure (d1), at room temperature without daylight  
612 exposure (d2), at refrigerated conditions (d3). Scanning electron micrographs of AMBR2  
613 spray-dried powders after 28 weeks of shelf-life dried in nitrogen: unprotected cells kept at  
614 room temperature with daylight exposure (e1), at room temperature without daylight exposure  
615 (e2), at refrigerated conditions (e3), 1% SM formulation cells kept at room temperature with  
616 daylight exposure (f1), at room temperature without daylight exposure (f2), at refrigerated  
617 conditions (f3), 10% SM formulation cells kept at room temperature with daylight exposure  
618 (g1), at room temperature without daylight exposure (g2), at refrigerated conditions (g3), 20%  
619 SM formulation cells kept at room temperature with daylight exposure (h1), at room  
620 temperature without daylight exposure (h2), at refrigerated conditions (h3).

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